



**B.TECH DEGREE EXAMINATIONS: MAY 2015**

(Regulation 2009)

Sixth semester

**BIOTECHNOLOGY**

BTY118: Bioprocess Engineering

**Time: Three Hours**

**Maximum Marks: 100**

**Answer all the Questions:-**

**PART A (10 x 1 = 10 Marks)**

- $k_L a$  can be measured by sulphite oxidation method. The DO concentration measured by probe in sodium sulphite solution will be.  
a) Zero  
b) Maximum  
c) Constant  
d) Minimum
- The major problems associated with turbidity measurements in bioreactors are.  
a) Fouling from gas bubbles  
b) Interference from gas bubbles  
c) Both a & c  
d) Accumulation of cells in turbidity sensors
- In RTD measurement techniques, multiple peaks are obtained for PFR due to.  
a) Short circuiting  
b) Ineffective utilization of reactor volume  
c) Internal recirculation  
d) By-passing
- The solubility of oxygen \_\_\_\_\_ with increase in temperature.  
a) Decrease  
b) No change  
c) Increase  
d) Maximum
- The following items consist of two statements, one labeled as the "Assertion (A)" and the other as "Reason (R)". You are to examine those two statements carefully and select the answers to these items using the codes given below:

Assertion (A): During fermentation, cells suffer inhibitory effects from exposure to very high oxygen partial pressure

Reason(R) : Pure oxygen increases  $k_L a$  value

Codes:

- Both A and R are individually true and R is the correct explanation of A
- Both A and R are individually true but R is not the correct explanation of A
- A is true but R is false
- A is false but R is true



concentration of  $5 \times 10^{12} \text{ m}^{-3}$ ; the activation energy and Arrhenius constant for thermal destruction of these contaminants are  $283 \text{ kJ.mol}^{-1}$  and  $5.7 \times 10^{39} \text{ h}^{-1}$ , respectively. A contamination risk of one organism surviving every 30 days operation is considered acceptable. The sterilizer pipe has an inner diameter of 30 cm; the length of the holding section is 12 m. The density of the medium is  $1000 \text{ kg.m}^{-3}$  and the viscosity is  $3.6 \text{ kg.m}^{-1}.\text{h}^{-1}$ . What sterilizing temperature is required?

**(OR)**

- b) Describe how the ills of a flow bioreactor can be diagnosed using tracer studies. Substantiate your answer with neat diagram.

22. a) Derive an expression for scale-up of a bioreactor using the following criteria:
- (i) Constant power per unit volume. (5)
  - (ii) Constant  $K_L a$ . (5)
  - (iii) Constant impeller tip speed. (4)

**(OR)**

- b) A strain of *Azotobacter vinelandii* is cultured in a  $15 \text{ m}^3$  stirred fermenter for alginate production. Under current operating conditions,  $k_L a$  is  $0.17 \text{ s}^{-1}$ . Oxygen solubility in the broth is approximately  $0.008 \text{ kg.m}^{-3}$ .
- (i) The specific rate of oxygen uptake is  $12.5 \text{ mmol.g}^{-1}.\text{h}^{-1}$ . What is the maximum possible cell concentration? (7)
  - (ii) The bacteria suffer growth inhibition after copper sulphate is accidentally added to the fermentation broth. This causes a reduction in oxygen uptake rate to  $3 \text{ mmol.g}^{-1}.\text{h}^{-1}$ . What maximum cell concentration can now be supported by the fermenter? (7)

23. a) With a neat diagram, explain the working principle, application of flow injection analysis. Substantiate your answer with biotechnological application.

**(OR)**

- b) How do you calculate the heat evolved during fermentation?

24. a) Consider industrial scale batch fermentation. A 10,000 L fermenter with  $5 \times 10^{10}$  cells/ml is the desired scaleup operation. Inoculum of the large tank is brought through a series of seed tanks and flasks, beginning with a single pure colony growing on a agar slant. Assume that a colony ( $10^6$  plasmid containing cells) is picked and placed in a test tube with 1 mL of medium. Calculate how many generations will be required to achieve the cell density in the 10,000l fermenter. What fraction of the total population will be plasmid-free cells if  $\mu_+ = 1.0\text{h}^{-1}$ ,  $\mu_- = 1.2\text{h}^{-1}$  and  $P = 0.0005$ .

**(OR)**

- b) Derive an expression for plasmid instability model for batch fermentation.

25. a) Explain the importance of structured models in analysis of various bioprocesses.

**(OR)**

- b) With a neat diagram, describe the following

(a) Single cell model. (7)

(b) Compartment models. (7)

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