



**B.TECH DEGREE EXAMINATIONS: NOV/DEC 2022**

(Regulation 2018)

Fifth Semester

**BIOTECHNOLOGY**

U18BTI5202 BIOPROCESS ENGINEERING

**COURSE OUTCOMES**

- CO1:** Apply the knowledge of various optimization methods to design the media for fermentation broth  
**CO2:** Evaluate the sterilization kinetics of media and able to design the holding time for batch sterilization  
**CO3:** Develop a suitable mathematical models for batch, fed-batch and continuous fermentation and able to simulate and evaluate the constants for microbial growth  
**CO4:** Understand and analyse the application of various bioreactors and importance of mass transfer effect in bioprocess engineering  
**CO5:** Apply the various scale-up criteria to design the bioreactors  
**CO6:** Identify and provide the solution for non- ideal performance of bioreactor

**Time: Three Hours**

**Maximum Marks: 100**

**Answer all the Questions**  
**PART A (10 x 2 = 20 Marks)**  
**(Answer not more than 40 words)**

- |  |     |      |
|--|-----|------|
| 1. What do you mean by anti foaming agents?  | CO1 | [K2] |
| 2. Mention the disadvantages of medium optimization by classical methods   | CO1 | [K2] |
| 3. How do you avoid the contamination in fermentation process ?  | CO2 | [K3] |
| 4. List the two types of reaction contribute to the loss of nutrient quality during sterilization.                                       | CO2 | [K2] |
| 5. What problems could be caused by the growth of contaminants during fermentation ?   | CO3 | [K3] |
| 6. Suggest how to reduce the lag phase in batch fermentation   | CO3 | [K3] |
| 7. How much factor of solubility of oxygen increases when sparing pure oxygen instead of air at the same total pressure and temperature? | CO4 | [K4] |
| 8. Enlist the factors influencing the value of 'a' oxygen transfer in shake flake.   | CO4 | [K3] |
| 9. Enlist the major factors affecting the scale-up process   | CO5 | [K3] |
| 10. What do you mean by residence time distribution (RTD)?   | CO6 | [K2] |

**Answer any FIVE Questions:-**  
**PART B (5 x 16 = 80 Marks)**  
**(Answer not more than 400 words)**

- |        |   |    |     |                   |
|--------|---|----|-----|-------------------|
| 11. a) | Using the Plackett-Burmann Design for media containing seven variables. Identify the key variable affecting the optimization of media. Consider the D and G as dummy variables. Comment on your prediction. | 10 | CO1 | [K <sub>5</sub> ] |
|--------|---|----|-----|-------------------|

Experiments	A	B	C	D	E	F	G	Enzyme activity
1	H	H	H	L	H	L	H	2.3
2	L	H	H	H	L	H	L	12.3

3	L	L	H	H	H	L	H	2.4
4	H	L	L	H	H	H	L	1.6
5	L	H	L	L	H	H	H	12
6	H	L	H	L	L	H	H	2
7	H	H	L	H	L	L	L	2.1
8	L	L	L	L	L	L	L	2.8

b) Enumerate the serum free media supplements used animal cell culture 6 CO1 [K<sub>2</sub>]

12. a) The number of viable spores of a new strain of *Bacillus subtilis* is measured as a function of time at various temperatures 16 CO2 [K<sub>4</sub>]

Time (min)	Number of spores			
	T = 85°C	T = 90°C	T = 110°C	T = 120°C
0.0	2.40 x 10 <sup>9</sup>			
0.5	2.39 x 10 <sup>9</sup>	2.38 x 10 <sup>9</sup>	1.08 x 10 <sup>9</sup>	2.05 x 10 <sup>9</sup>
1.0	2.37 x 10 <sup>9</sup>	2.30 x 10 <sup>9</sup>	4.80 x 10 <sup>9</sup>	1.75 x 10 <sup>9</sup>
1.5	-	2.29 x 10 <sup>9</sup>	2.20 x 10 <sup>9</sup>	1.30 x 10 <sup>9</sup>
2.0	2.33 x 10 <sup>9</sup>	2.21 x 10 <sup>9</sup>	9.85 x 10 <sup>9</sup>	-
3.0	2.32 x 10 <sup>9</sup>	2.17 x 10 <sup>9</sup>	2.01 x 10 <sup>9</sup>	-
4.0	2.23 x 10 <sup>9</sup>	2.12 x 10 <sup>9</sup>	4.41 x 10 <sup>9</sup>	-
6.0	2.20 x 10 <sup>9</sup>	1.95 x 10 <sup>9</sup>	1.62 x 10 <sup>9</sup>	-
8.0	2.19 x 10 <sup>9</sup>	1.87 x 10 <sup>9</sup>	6.68 x 10 <sup>9</sup>	-
9.0	2.16 x 10 <sup>9</sup>	1.79 x 10 <sup>9</sup>	-	-

- i. Determine the activation energy for thermal death of *B.subtilis* spores
- ii. Calculate the specific growth rate at 100°C
- iii. Estimate the time required to kill 99% of spores in a sample at 100°C

13. a) Design a bioreactor for the growth of a single cell protein. Emphasis on the setup, and harvest protocols in detail 16 CO3 [K<sub>6</sub>]

14. a) With a neat diagram, explain in detail about how an oxygen from gas bubble is transfer to cells. 8 CO4 [K<sub>3</sub>]

b) A stirred fermenter is used to culture haematopoietic cells isolated from umbilical cord blood. The liquid volume is 15 litres. The simple dynamic method is used to determine k<sub>L</sub>a. The air flow is shut off for a few minutes and the dissolved oxygen level drops; the air supply is then reconnected 8 CO4 [K<sub>5</sub>]

at a flow rate of 0.25 L/s. The following results are obtained at a stirrer speed of 50 rpm. When steady state is established, the dissolved oxygen tension is 78% air saturation. In separate test experiments, the electrode response to a step change in oxygen tension did not vary with stirrer speed above 40 rpm. The probe response time under these conditions was 2.8 s. When the  $k_L a$  measurement was repeated using nitrogen sparging to deoxygenate the culture, the results for oxygen tension as a function of time were similar to those listed.

Estimate  $k_L a$ .

<b>Time (second)</b>	5	20
<b>Oxygen tension (% air saturation)</b>	50	66

15. a) Consider the scale-up of a fermentation from a 10 L to 10,000 L vessel. The small fermenter has a height-to-diameter ratio of 3. The impeller diameter is 30% of the tank diameter. Agitator speed is 500 rpm and three Rushton impellers are used. Determine the dimensions of the large fermenter and agitator speed for: 10 CO5 [K<sub>5</sub>]
- i. Constant  $P/V$
  - ii. Constant impeller tip speed
  - iii. Constant Reynolds number
- b) Enlist the factors affecting the scale-up process. 6 CO5 [K<sub>2</sub>]
16. a) Describe the how the ills of flow bioreactors can be diagnosed using tracer studies. Substantiate your answer with neat diagram 16 CO5 [K<sub>3</sub>]

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